



# Commercialization of the Iron-Based Coal Direct Chemical Looping Process for Power Production with In Situ Carbon Dioxide Capture

Luis Velazquez-Vargas

# Project Participants

## ▶ Federal Agencies:

- DOE/NETL

## ▶ State Agency

- Ohio Development Services Agency

## ▶ Industry & University

- The Babcock & Wilcox Company (B&W)
- The Ohio State University (OSU)
- Clear Skies Consulting
- Johnson Matthey (JM)
- EPRI
- Dover Light & Power
- Nexant
- American Electric Power
- Dayton Power & Light
- Duke Energy
- First Energy
- CONSOL Energy



Development  
Services Agency



Clear Skies  
Consulting



# Project Overview

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**NETL**

**Pilot PHASE I**

Year: 2012-2013

- Design of 550 MWe commercial CDCL power plant
- Techno-economic analysis
- Technology gap analysis

**NETL**

**Pilot PHASE II -A**

Year: 2013-2015

- Laboratory testing – cold flow model
- Design of pilot plant facility (250 kW<sub>th</sub>)
- Cost estimate and schedule for fabrication construction and testing of pilot facility

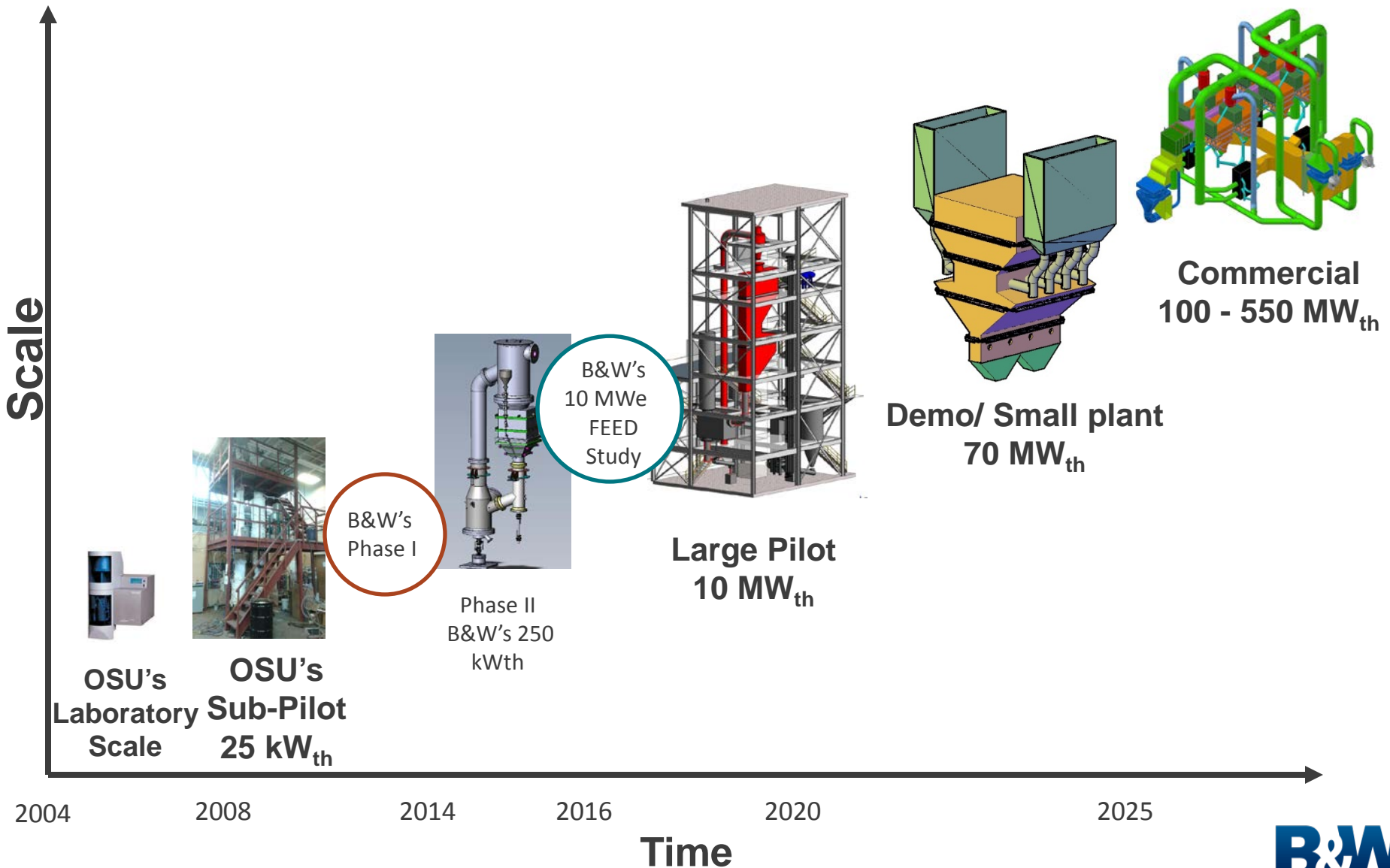
**NETL-ODSA**

**Pilot PHASE II-B**

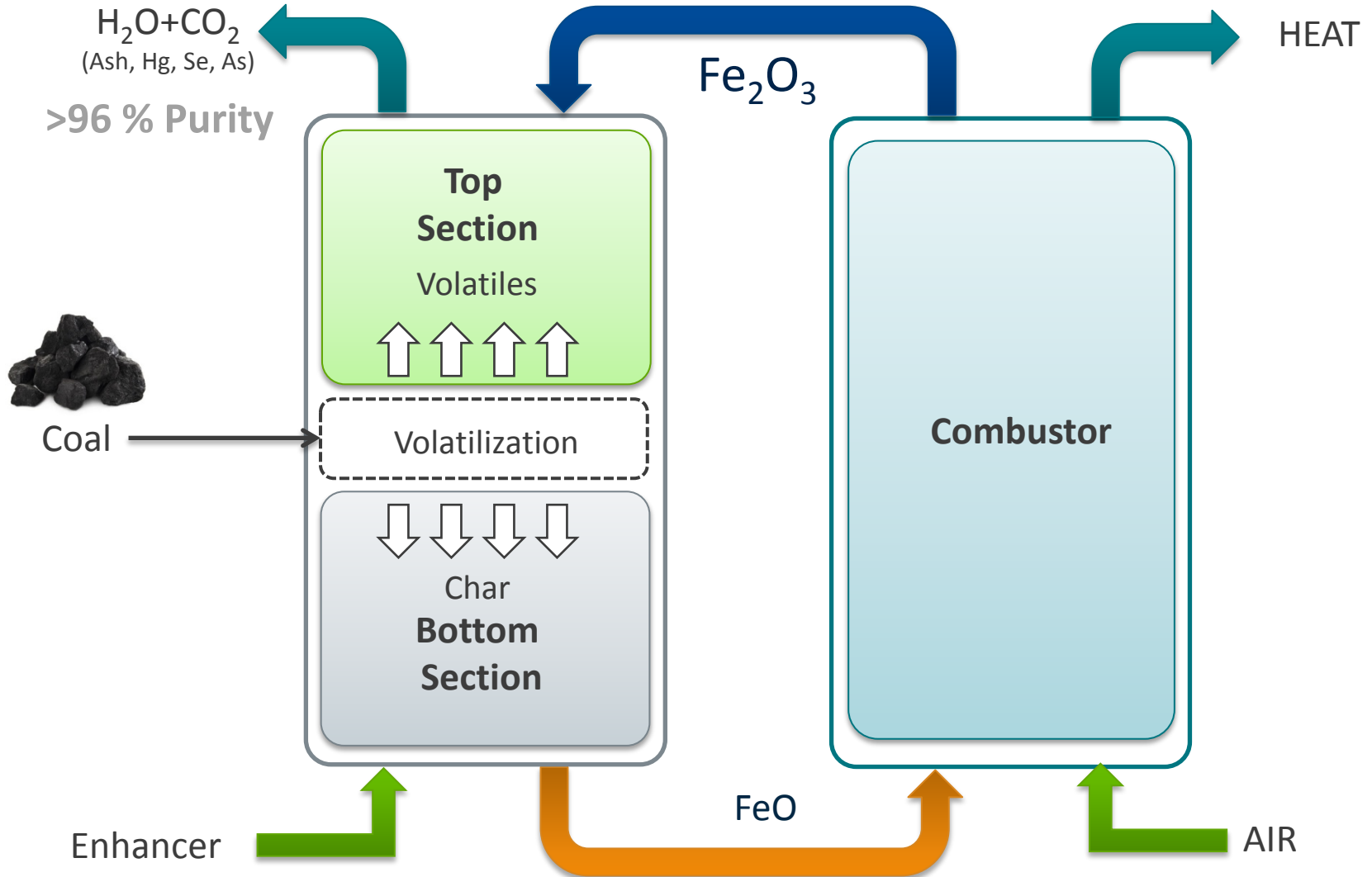
Year: 2015-2017

- Construction of CDCL pilot facility
- Testing of CDCL Pilot Unit
- Performance analysis and reporting
- Commercialization path – large-scale testing

# Coal Direct Commercialization Path

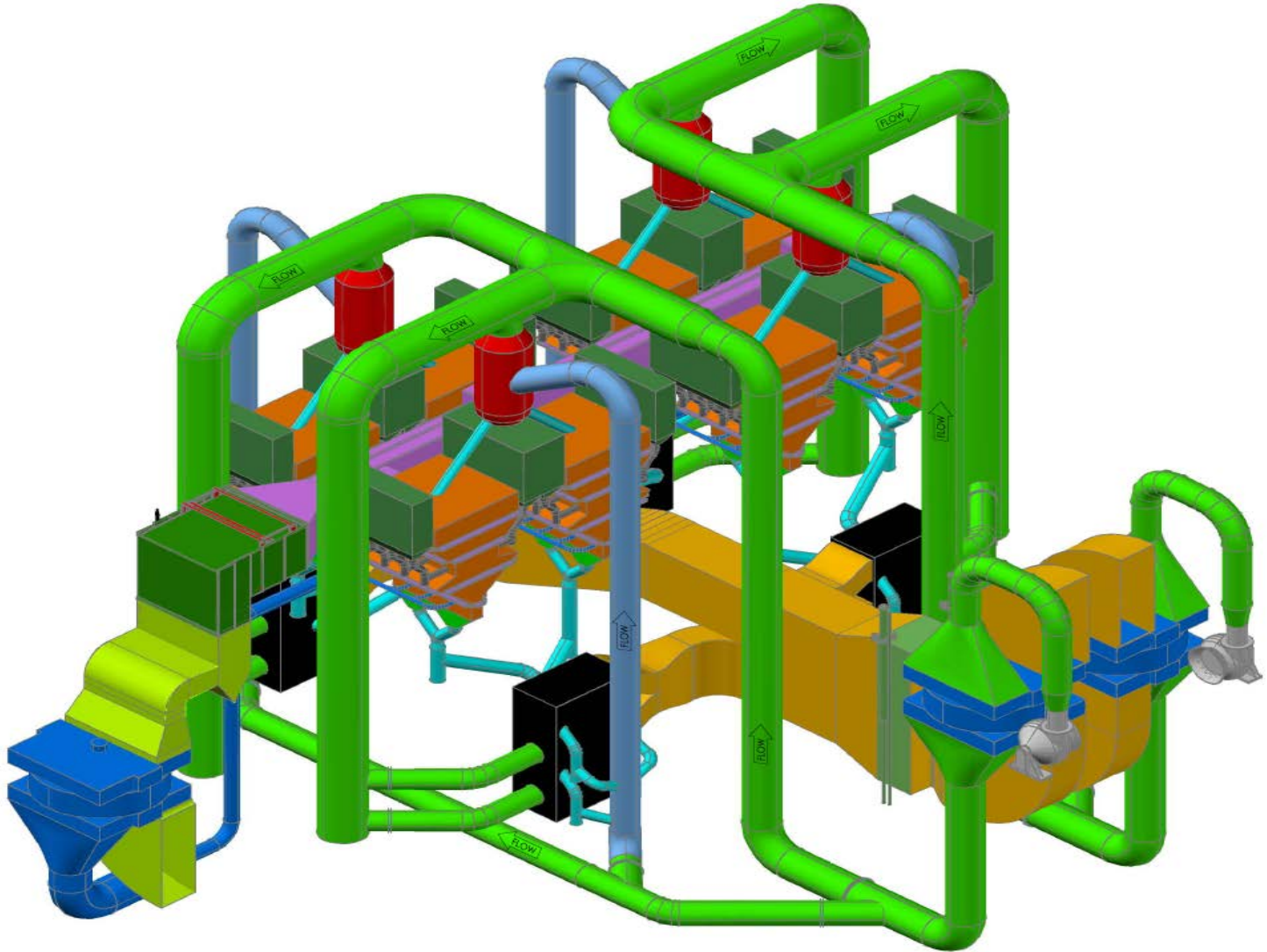


# CDCL Process Overview



# CDCL Commercial Plant Design and Engineering

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# Phase I: Technology Gap Analysis

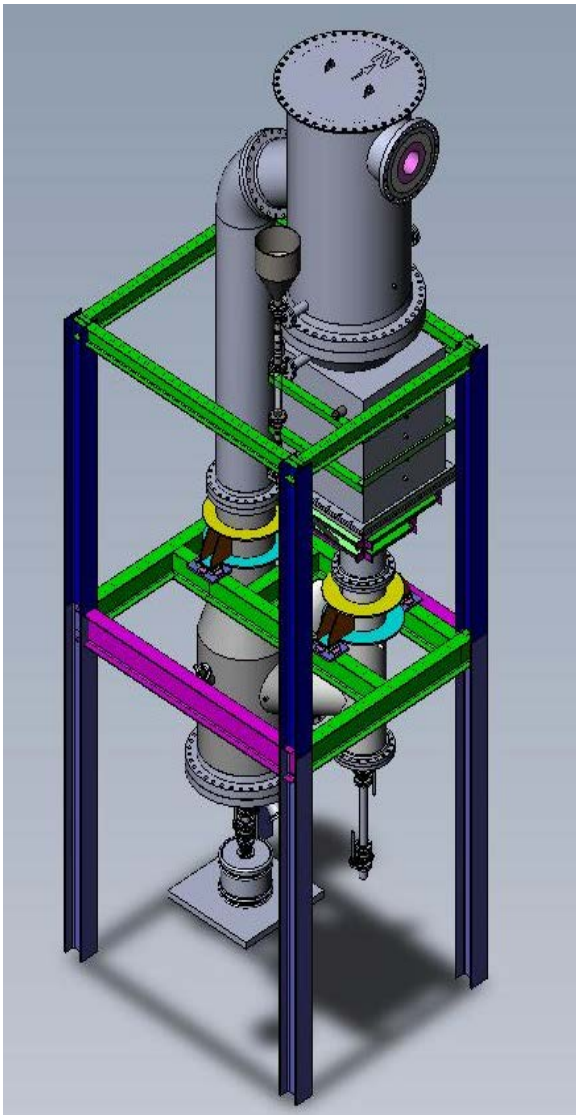
Design/Technology Issues	Ongoing/Past Mitigation	Planned Mitigation	Future Mitigation
<b>Particles</b>			
Manufacturing Cost	Under OSU's Scope	Particle Manufacturer (JM)	Multiple Manufacturers
Attrition	250 kWth / NCCC	Attrition Tests / 250 kWth	10 MWe Large Pilot
High Temperature Resistance	TGA	TGA / 250 kWth	10 MWe Large Pilot
<b>Reducer</b>			
Coal Injection & Distribution	25 kWth Sub-Pilot	Coal RXN Model / 250 kWth	10 MWe Large Pilot
Char Residence Time	25 kWth Sub-Pilot	Coal RXN Model / 250 kWth	10 MWe Large Pilot
Ash Separation / Enhancer Gas	CFM / 25 kWth Sub-Pilot	CFM / 250 kWth	10 MWe Large Pilot
Char Carryover	CFM / 25 kWth Sub-Pilot	CFM / 250 kWth	10 MWe Large Pilot
Pressure Drop	Phase I / 25 kWth Sub-Pilot	250 kWth	10 MWe Large Pilot
CO <sub>2</sub> Purity	25 kWth Sub-Pilot	250 kWth	10 MWe Large Pilot
Sulfur, NO <sub>x</sub> , Hg Emissions	25 kWth Sub-Pilot	Small-pilot Unit	10 MWe Large Pilot
Alkaline Management	2" BFB Studies	2" BFB Studies	10 MWe Large Pilot
<b>Combustor</b>			
Heat Exchanger surface	B&W's CFB Technology	B&W's CFB Technology	10 MWe Large Pilot
Auto-thermal Operation	Phase I (Calculation)	250 kWth	10 MWe Large Pilot
<b>Process</b>			
Operation	25 kWth Sub-Pilot / NCCC	250 kWth	10 MWe (modular)
Start up/Shut down	25 kWth Sub-Pilot / NCCC	250 kWth	10 MWe (modular)
Safety	25 kWth Sub-Pilot / NCCC	250 kWth	10 MWe (modular)

# CDCL Technology Comparison

	Base Plant	MEA Plant	CDCL Plant
Coal Feed, kg/h	185,759	256,652	205,358
CO <sub>2</sub> Emissions, kg/MWh <sub>net</sub>	801	111	31
CO <sub>2</sub> Capture Efficiency, %	0	90	96.5
Net Power Output, MW <sub>e</sub>	550	550	550
Net Plant HHV Heat Rate, kJ/kWh (Btu/kWh)	9,165 (8,687)	12,663 (12,002)	10,084 (9,558)
Net Plant HHV Efficiency, %	39.3	28.5	35.6
Cost of Electricity, \$/MWh	80.96	132.56	102.67
Increase in Cost of Electricity, %	-	63.7	26.8



# Phase II: 250 KW<sub>th</sub> Pilot Unit Design



## Pilot Design:

- Reducer Design
- Material and Energy Balances
- Support Structure Design
- Detail Construction Drawings

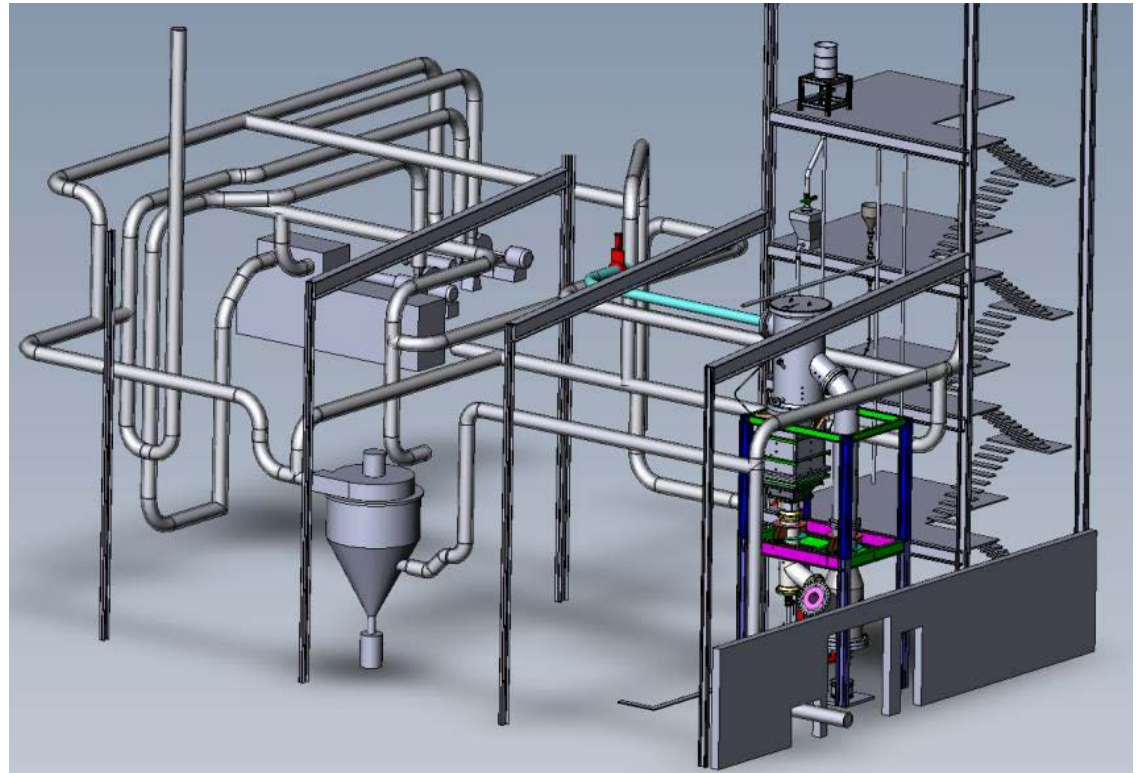
## Specifications

- Materials: Refractory lined Carbon Steel
- Overall Height: 32 ft
- Footprint = 10' x 10'
- Thermal rating: 250 kW<sub>th</sub>
- Coal Feed Rate: 70 lb/hr
- Coal size: Pulverized coal
- Max Operating Temperature: 2012 °F
- Oxygen Carrier: Iron based
- Reducer : Counter-current moving bed
- Combustor : Bubbling bed
- Particle transport: Pneumatic
- Active metal: Iron based
- Size: 1.5 mm

# Phase II: 250 KW<sub>th</sub> Pilot Plant Facility Design

## Pilot Plant Facility Design

- Auxiliary Equipment Specifications
  - Coal Handling
  - Gas Heating, Cooling & Cleanup
  - Ash and Oxygen Carrier Handling Equipment
- P&ID Diagrams
- HazOp Analysis
- Equipment Specifications
- Control Specifications
- Cost Estimate
- Fabrication, Construction and Installation Schedules

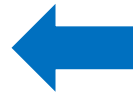


# Phase II: 250 KW<sub>th</sub> Pilot Fabrication





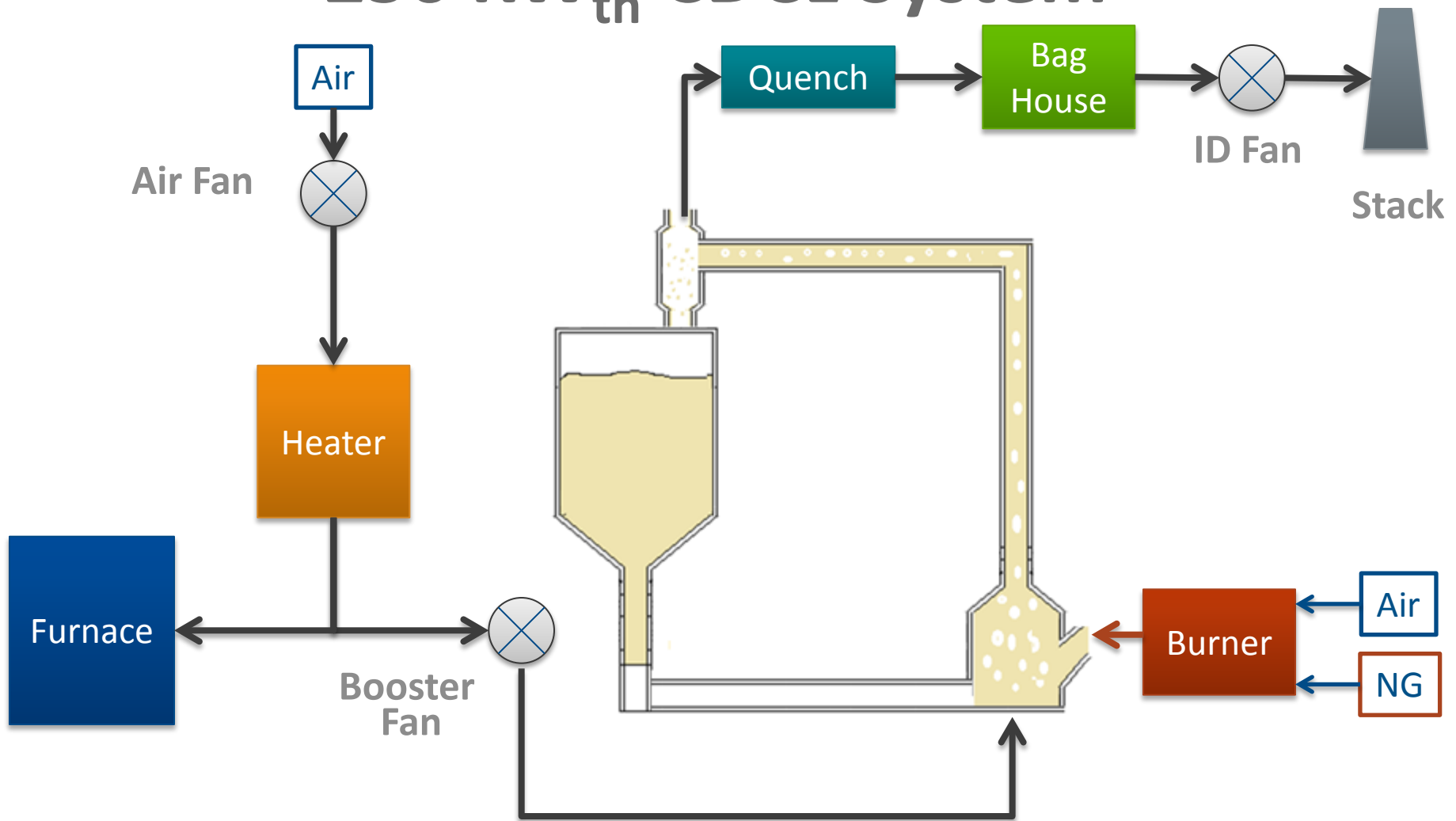
# Phase II: 250 kW<sub>th</sub> Pilot Construction & Installation



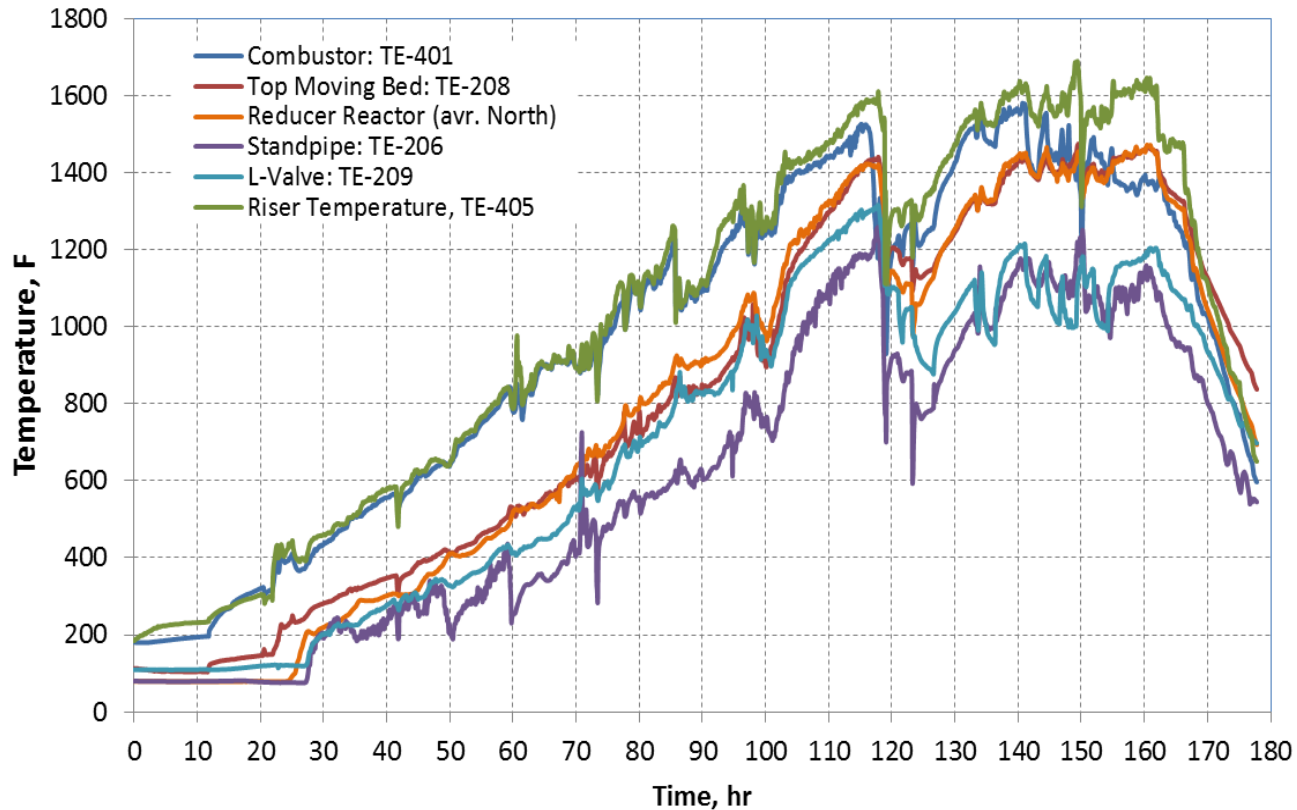
# Phase II: 250 kW<sub>th</sub> Pilot Construction & Installation



# 250 KW<sub>th</sub> CDCL System

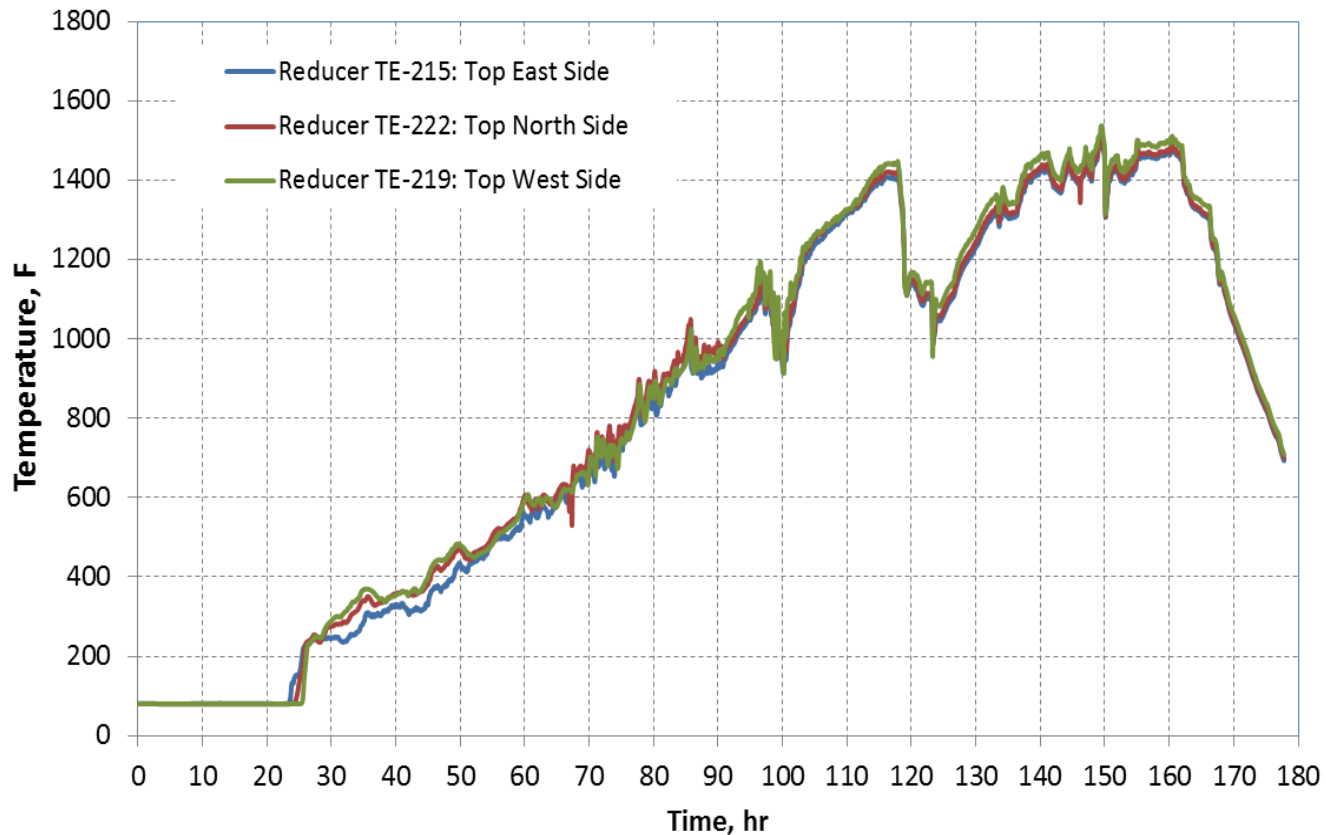


# 250 kW<sub>th</sub> CDCL Pilot Plant Test Results



Refractory Bake-Out (March-2017)

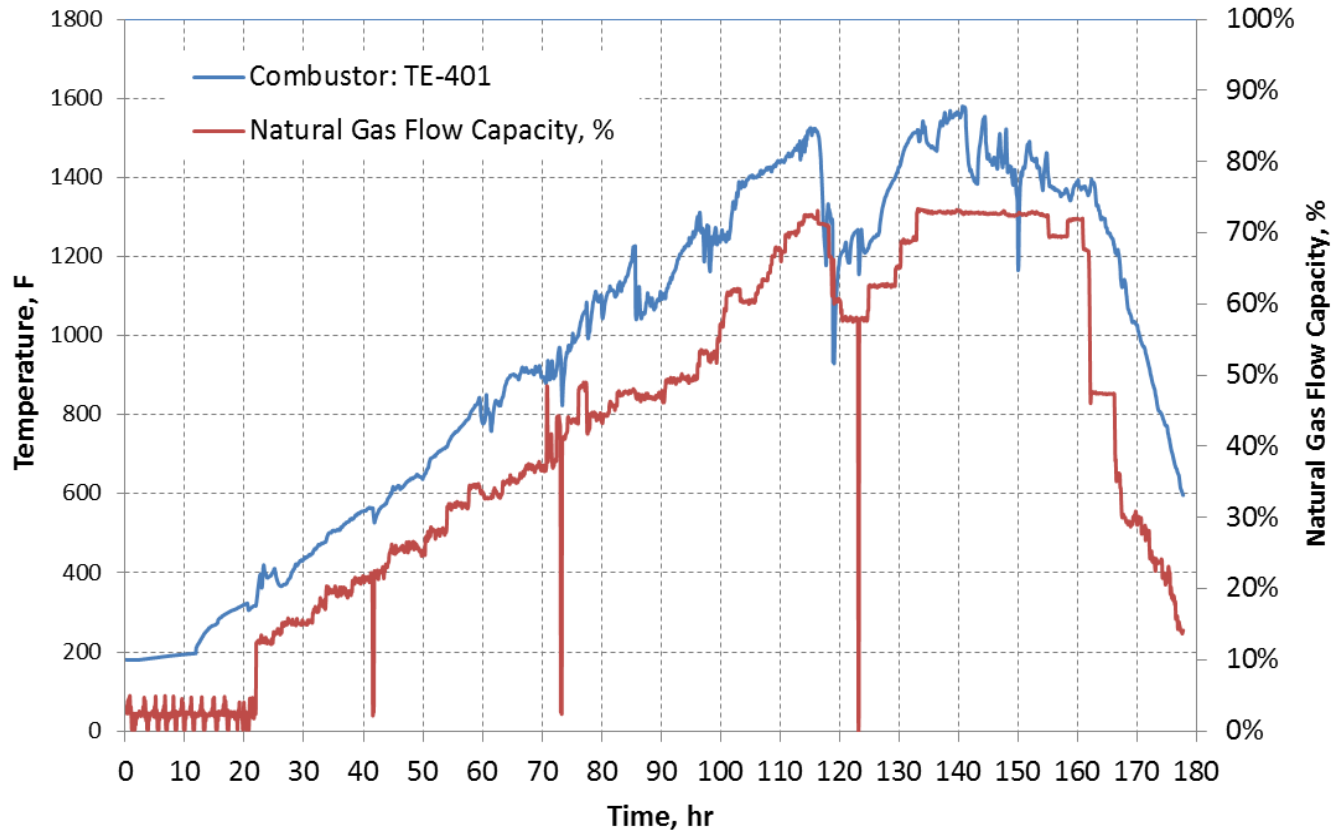
# 250 kW<sub>th</sub> CDCL Pilot Plant Test Results



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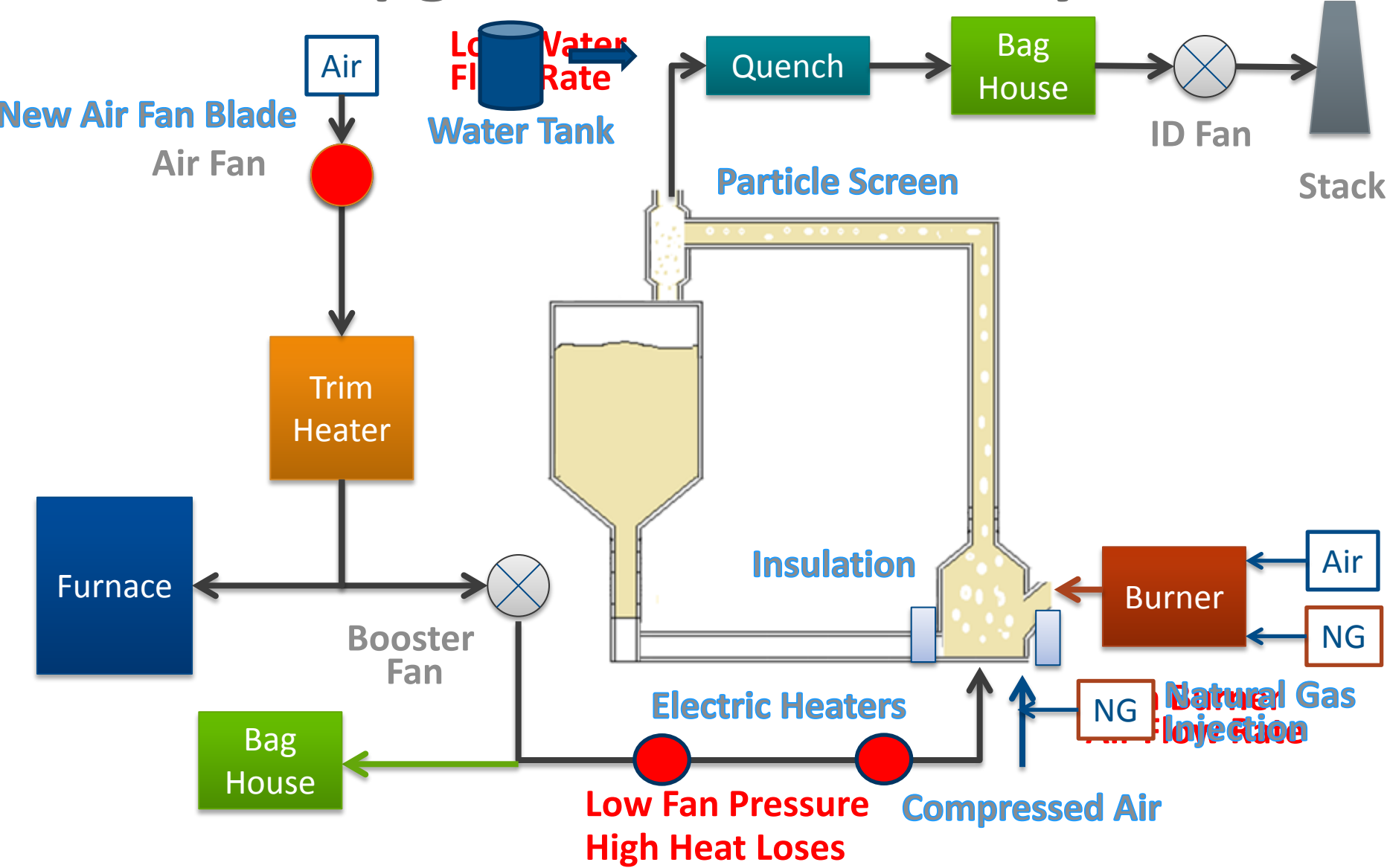


# 250 kW<sub>th</sub> CDCL Pilot Plant Test Results

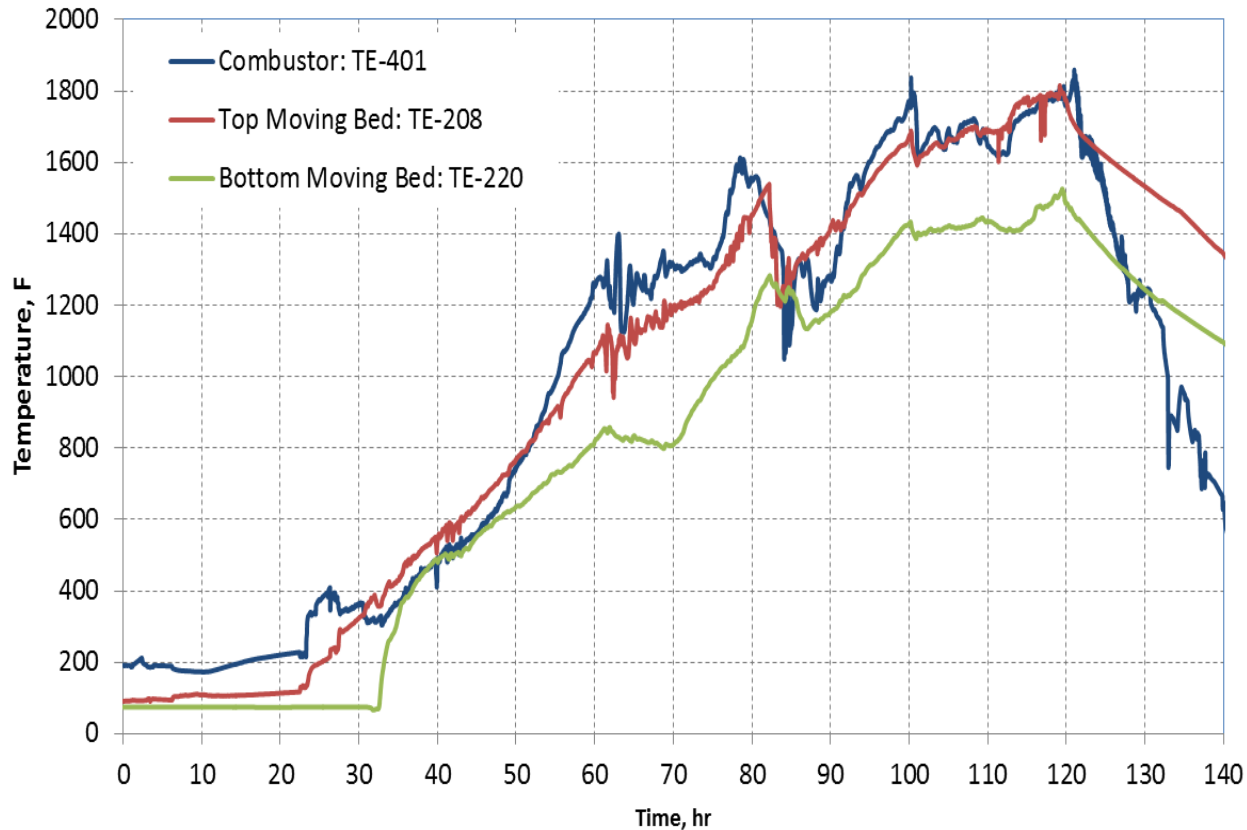


Refractory Bake-Out (March-2017)

# Upgrades to the facility

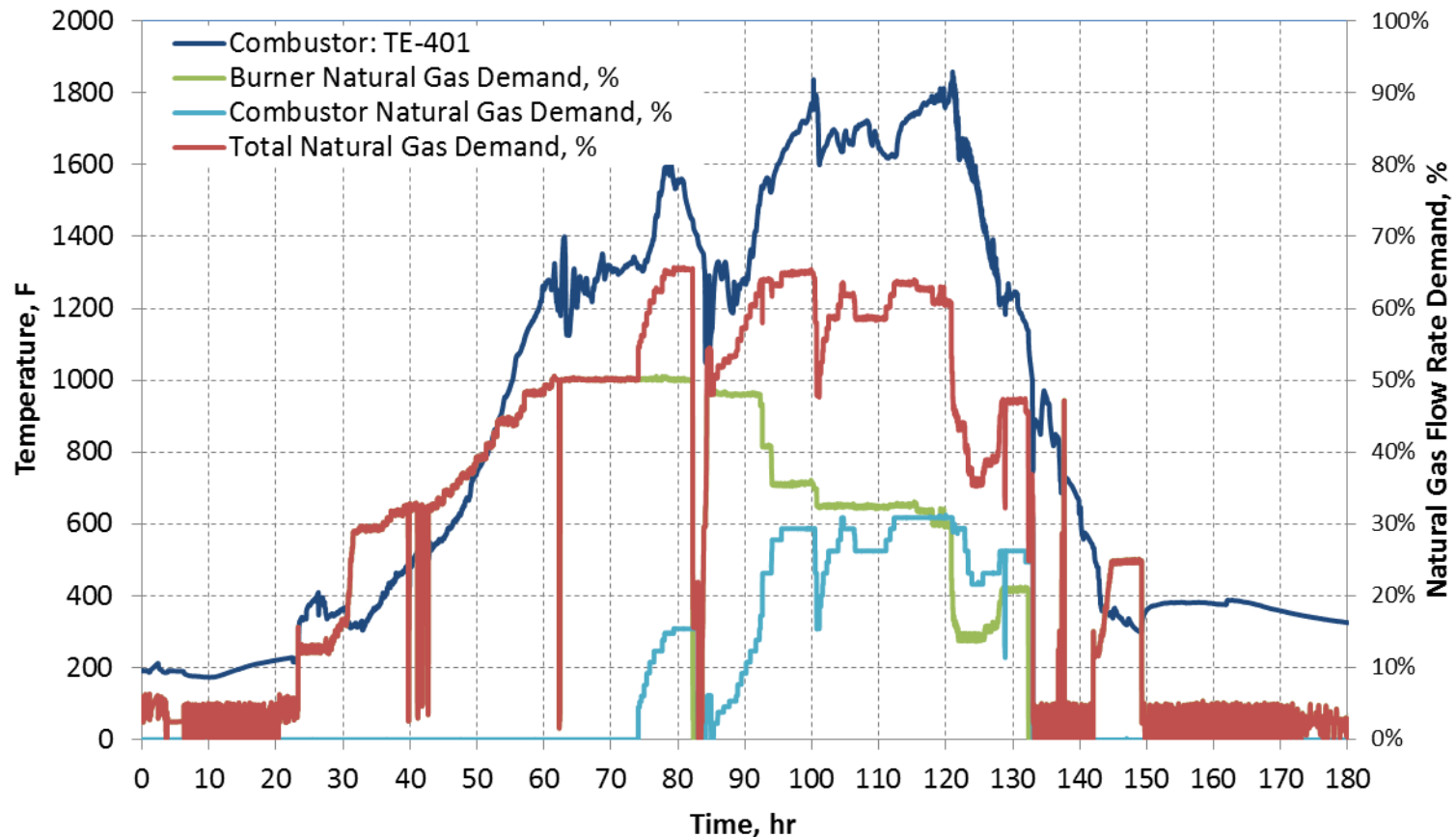


# 250 kW<sub>th</sub> CDCL Pilot Plant Test Results



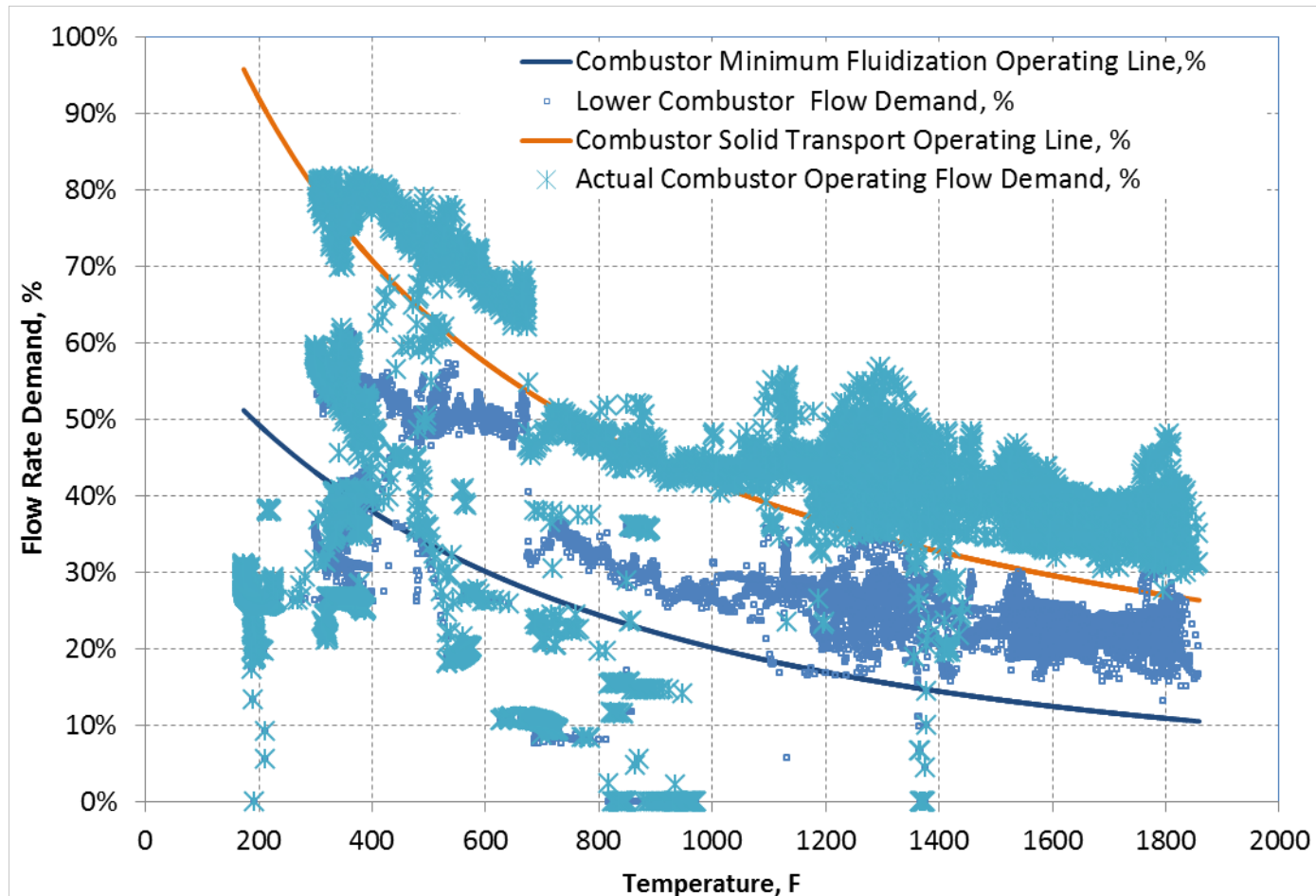
Second Test Run (June-2017)

# 250 kW<sub>th</sub> CDCL Pilot Plant Test Results



Second Test Run (June-2017)

# 250 kW<sub>th</sub> CDCL Pilot Plant Test Results



Second Test Run (June-2017)

# Conclusions

- ▶ CDCL Process represents a 2<sup>nd</sup> generation oxyfuel combustion technology capable of substantially reducing the cost of electricity increase associated with CO<sub>2</sub> capture
- ▶ Phase II 250 kW<sub>th</sub> pilot plant design, construction and commissioning activities are complete
  - Operating temperature for coal injection (~1,800°F) achieved
  - Initial coal testing shows nearly 100% CO<sub>2</sub> purity in flue gas
  - Over 200 hours of operation in two separate runs (>100 hours each)
  - Flue gas cooler / quench unit design verified & improved
  - Particle make-up & coal feed systems demonstrated & calibrated

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B&W Lead Operators

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